AMENDMENTS TO THE SPECIFICATION

Please replace the paragraph beginning at page 4, line 21, and ending at page 4, line 33, with the following:

---Reference is now made to Figure 1. Figure 1 shows an apparatus 10 for carrying out the process of the present invention. The apparatus 10 comprises a first vessel 12. The contaminant removed in the first vessel 12 is water and thus the gas exiting the first vessel 12 is dry. Also heavy hydrocarbons are removed as a consequence of this process, and thus the gas stream exiting the first vessel 12 is dew pointed for hydrocarbons to an [[extend]] extent determined by the conditions in the first vessel 12. The water dew point of the gas exiting the first vessel 12, however, is lower than its equilibrium dew point due to the formation of hydrates.---

Please replace the paragraph beginning at page 7, line 18, and ending at page 8, line 2, with the following:

---The dry sour gas at a pressure of 10 to 30 bar lower than the pressure upstream of the expansion device 24 and at the operating temperature of the first vessel [[14]] 12 is directed via second heat exchanger 36 in conduit 35 to a second flash tank 40. It is cooled in the second heat exchanger 36 to form a two-phase mixture of gas and condensate at a temperature higher than -56 °C. Not shown is that additional cooling may be provided by indirect heat exchange with a refrigerant that is circulated through an external refrigeration cycle, for example a propane refrigeration cycle. In the second flash tank 40, condensate is separated from the dry sour gas stream. The liquid stream exits the second flash tank 40 via liquid outlet 42 and is sufficiently cooled to satisfy the criteria of a sub-cooled liquid that may be fed to the sub-cooled liquid inlet 26 of the first vessel 12. The sub-cooled liquid is supplied through conduit 43, provided with a pump 44 to the sub-cooled liquid inlet 26.---

Please replace the paragraph beginning at page 8, line 3, and ending at page 8, line 6, with the following:

---The dry sour gas exits the second flash tank 40 via gas outlet [[44]] 47 and is fed through conduit 45 to the intermediate heat exchanger 22 and from there to an end user (not shown). Conduit 45 may comprise a Joule-Thompson valve 48.---

Please replace the paragraph beginning at page 9, line 14, and ending at page 9, line 28, with the following:

---The dry sour gas exits the second flash tank 40 via gas outlet [[44]] 47 and is fed to a second vessel 14 via dry sour gas inlet 46. As with the first vessel 12, the dry sour gas being fed to the second vessel 14 may be expanded through a Joule-Thompson valve 48 or other suitable expansion means, such as a turbo expander, in order to further cool the gas. As before with the first vessel 12, the Joule-Thompson valve may define the dry sour gas inlet 46. The temperature of the dry gas entering into the second vessel 14 is at a second operating temperature. The second operating temperature is the maximum temperature at which solids of the sour species are formed or the temperature at which the sour species dissolve in a liquid.---

Please replace the paragraph beginning at page 11, line 3, and ending at page 11, line 10, with the following:

---Suitably, the sub-cooled liquid is part of the liquid passing through conduit 43. In order to reduce the temperature the liquid is passed through conduit 50 to the heat exchanger 38 where it is cooled by indirect heat exchange with dry sweetened gas. The dry sweetened gas is then passed through conduit 65 to heat exchanger 36 for cooling the dry sour gas from the first vessel 12. The dry sweetened gas is then fed to the intermediate heat exchanger 22 and from there to an end user (not shown).---